

8/15/97	KRH	5. Connect the H <sub>2</sub> , O <sub>2</sub> , and N <sub>2</sub> supply lines to their respective tanks of compressed gas.	
8/16/97	KRH	6. Start the test using the start-up procedure found in Test Stand Start-up/shutdown Procedure IOP FCP-970704.	
10:41 am	KRH	7. Adjust the exhaust valves until the initial exhaust pressures.	See note 1.
10:41 am	KRH	8. Wire the fuel cell in parallel and connected to the 1-ohm load.	
11:00		9. Start recording data on the <u>Stack Experiment Membrane Conditioning</u> form FRM FCP-970804.	The data will be collected every half-hour. See note 2.
/		10. Calculate which load is producing the most power. Adjust the potentiometer so the fuel cell is producing the maximum power.	See note 3.
/		11. Repeat steps 7 and 8 every half-hour; continue until the fuel cell has operated for 8 hours.	
/		12. Conduct the <u>General Stack</u> experiment for one data set.	
<del>3:17</del> 3:17	KF	13. Finish the experiment with the shutdown procedure found in Test Stand Start-up/shutdown Procedure IOP FCP-970704.	
3:25	KRH	14. Disconnect the supply lines from the inlet lines for the H <sub>2</sub> , O <sub>2</sub> , and N <sub>2</sub> .	OK to leave connect if experiment will be continue another day
		15. Before leaving make sure that the test stand is in a safe condition.	
		16. Prepare a graph showing volts versus current density	See note 4.

8/16

yes

Notes

1. To acquire the proper exhaust pressure the rotameters should be fully opened and the regulators adjusted greater than the exhaust pressure.
2. The data is recorded by the following method.
  - Record time
  - Record the values of rotameters, hydration temperatures, thermocouples 1-4
  - Record the voltage across the 1-ohm load. Change the load to 5-ohms and wait a few seconds until the voltage settles and record voltage. Repeat for the 10, 25, 35, 50, 65, 80, & 100-ohms loads.
3. From the voltages recorded from step 7 calculate the power produced by the fuel cell by the following equation:

$$P = V^2 / R$$

Adjust the load across the fuel cell to that which is dissipating the most power.

4. Calculate the size of the reaction area of the total stack (cells wired in parallel) in  $\text{cm}^2$  and divide into the current output of the stack. The result will be the amount of current per  $\text{cm}^2$  or current density. Then plot voltage versus current density.

total area =  $1.9 \times 1.9 \text{ cm}^2$   
total area =  $3.61 \text{ cm}^2$   
 $1.9 \times 1.9 = 3.61$

## Stack Experiment: Membrane Preconditioning

Date: 8/16/97 Start Time: 11:00 am Finish Time: 12:00 pm

Persons Conducting Experiment Karin Fleckner Kevin Hanger

	1	2	3
time	11:00 am	11:30 am	12:00
H <sub>2</sub> , pressure, psi Exhaust	5	5.1	5.0
O <sub>2</sub> , pressure, psi Exhaust	8	8.1	7.6
H <sub>2</sub> , Rotameter, %	≈ 55	50	65
O <sub>2</sub> , Rotameter, SCFM (air)	5	2.5	6
H <sub>2</sub> , Hydration temp., °C	72.6	75.7	74.5
O <sub>2</sub> , Hydration temp., °C	69.0	73.6	72.0
Thermocouple 1, °C H <sub>2</sub> Exhaust	64.0	68.3	69.4
Thermocouple 2, °C O <sub>2</sub> Exhaust	64.2	69.0	73.5
Thermocouple 3, °C Water Bath	76.3	81.5	80.8
Thermocouple 4, °C Air Temp in stack	22.8	22.8	22.8

Resistance load, ohms R	10 <sup>-3</sup>		10 <sup>-3</sup>		10 <sup>-3</sup>	
	Volts V	Power V <sup>2</sup> /R	Volts V	Power V <sup>2</sup> /R	Volts V	Power V <sup>2</sup> /R
1	0.037	1.369	0.038	1.444	0.035	1.225
5	0.177	6.266	0.153	4.602	0.141	3.970
10	0.277	7.673	0.247	6.101	0.233	5.429
25	0.430	7.396	0.400	6.400	0.383	5.868
35	0.482	6.438	0.456	5.941	0.437	5.436
50	0.536	5.740	0.512	5.243	0.496	4.920
65	0.569	4.981	0.548	4.620	0.534	4.387
80	0.592	4.381	0.573	4.104	0.562	3.948
100	0.617	3.807	0.600	3.600	0.590	3.481

Comments: Note overall power drop from reading 1 to 2.

After measurement 2 Adjusted ~~changed~~ A<sub>2</sub> back to 5psi flow at 62%  
O<sub>2</sub> " " 7.5 flow at 6 SCFM

- Again: a drop from reading 2 to 3.

Poor connection at stack (adjust screws)

cells 2 & 3 open circuit voltage ≈ 0.45-0.5 volts  
" 1 & 4 " " " ≈ 0.815

after adjusting screws on 2 & 3 all cell were at ≈ 0.815 volt  
add H<sub>2</sub>O to O<sub>2</sub> hydration at 12:10 pm

## Stack Experiment: Membrane Preconditioning

Date: 8/16/97 Start Time: 12:30 pm Finish Time: 2:00

Persons Conducting Experiment Karen Fleckner Kevin Hoyer

Reading	4	5	6
time	12:30 pm	1:30	2:00
H <sub>2</sub> , pressure, psi	5	5	5
O <sub>2</sub> , pressure, psi	7.5	7.5	7.5
H <sub>2</sub> , Rotameter, %	65	65	65
O <sub>2</sub> , Rotameter, SCFM(air)	6.5	6	6
H <sub>2</sub> , Hydration temp., °C	73.6	72.5	73.1
O <sub>2</sub> , Hydration temp., °C	67.8	66.4	67.2
Thermocouple 1, °C	72.6	67.6	66.8
Thermocouple 2, °C	68.1	66.1	66.9
Thermocouple 3, °C	82.6	78.8	78.7
Thermocouple 4, °C	22.8	22.5	22.6

Resistance load, ohms R	10 <sup>-3</sup>		10 <sup>-3</sup>		10 <sup>-3</sup>	
	Volts V	Power V <sup>2</sup> /R	Volts V	Power V <sup>2</sup> /R	Volts V	Power V <sup>2</sup> /R
1	0.042	1.764	0.051	2.601	0.052	2.704
5	0.188	7.069	0.212	8.989	0.220	9.180
10	0.280	7.840	0.320	10.240	0.325	10.563
25	0.436	7.004	0.404	8.612	0.472	8.911
35	0.482	6.438	0.514	7.431	0.510	7.607
50	0.540	5.832	0.502	6.317	0.561	6.294
65	0.570	4.498	0.593	5.910	0.590	5.355
80	0.596	4.490	0.610	4.743	0.612	4.682
100	0.617	3.807	0.638	4.070	0.635	4.032

Comments: - power increase from reading 3 to 4 - after contact (electrical) were adjusted.

Skipped 1:00 measurement - O<sub>2</sub> Hydration water line needed fixed and DI water added

- Significant increase in power out - 10.240

## Stack Experiment: Membrane Preconditioning

Date: 8/16/97 Start Time: 2:33 Finish Time: 3:00

Persons Conducting Experiment \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

	1	4	9
time	2:30	2:40	3:00
H <sub>2</sub> , pressure, psi	5	5	5
O <sub>2</sub> , pressure, psi	7.6	7.8	7.5
H <sub>2</sub> , Rotameter, %	65	65	65
O <sub>2</sub> , Rotameter, SCFM(air)	6	6	6
H <sub>2</sub> , Hydration temp., °C	75.3	74.5	75.1
O <sub>2</sub> , Hydration temp., °C	70.0	69.2	67.0
Thermocouple 1, °C	73.9	75.6	75.9
Thermocouple 2, °C	69.4	70.0	70.7
Thermocouple 3, °C	83.2	83.8	84.0
Thermocouple 4, °C	22.7	22.7	22.6

Resistance load, ohms R	$10^{-3}$		$10^{-3}$		$10^{-3}$	
	Volts V	Power V <sup>2</sup> /R	Volts V	Power V <sup>2</sup> /R	Volts V	Power V <sup>2</sup> /R
1	0.059	3.481	0.069	4.761	0.063	3.099
5	0.211	8.909	0.212	9.00	0.212	9.50
10	0.315	9.923	0.316	9.99	0.316	9.986
25	0.463	8.575	0.463	8.575	0.465	8.649
35	0.515	7.578	0.512	7.490	0.515	7.578
50	0.560	6.272	0.556	6.183	0.558	6.227
65	0.593	5.410	0.586	5.283	0.587	5.351
80	0.616	4.743	0.610	4.651	0.611	4.667
100	0.636	4.045	0.630	3.970	0.632	3.994

Comments: Redo on 2:30 reading to verify power drop.

~~with cells in series & 10 ohm load.  
all cell~~

## Membrane Conditioning: Experiment 1

Date 8/18/97

Individuals conducting the experiment:

Karen Fleckner

Kevin Houser

### Purpose

The primary goal is to condition the membrane for maximum power output. Related to this goal is to develop the fastest method to condition membranes.

Secondary goals are to determine problems associated with the test stand, fuel cell stack, and the hydration systems so improvements may be made.

Discussions with experts and literature indicate that the membrane needs to be conditioned by operating under a load for about twelve hours before the membrane achieves maximum output. Maximum conditioning should occur at maximum power output. Over the initial conditioning period the maximum power output will vary with load. The four cells in the stack will remain connected in parallel during this experiment. Every half-hour the voltage will be measured across nine resistive loads (1,5,10,25,35,50,65,80,100 ohms) from which the power output of the fuel cell can be determined. Until the next measurement series the load which has the greatest power dissipation will be left connected to the fuel cell stack.

As with all experiments conducted on the test stand, fuel cell stack, and hydration systems, problems should be carefully recorded. If a solution is readily apparent it should also be noted.

### Apparatus and Materials

- Test Stand
- Assembled fuel cell stack.
- Hot water pump, heats and pumps water through the heated bath.
- (2) Variac
- Peristaltic pump

- Hydrogen gas cylinder
- Oxygen gas cylinder
- Nitrogen gas cylinder
- De-ionized water
- Stack Experiment: membrane Preconditioning (FRM FCP-970804) and Stack Experiment: General (FRM FCP-970712) forms as needed.

Initial Values

Variable	Setting desired
N <sub>2</sub> Regulator, psi	20
H <sub>2</sub> Regulator, psi	5 +
O <sub>2</sub> Regulator, psi	7.5 +
Hot Water Bath Temperature, °C	85
H <sub>2</sub> (Heating tape) variac, %	100
O <sub>2</sub> (Heating tape) variac, %	100
H <sub>2</sub> Rotameter, %	100
O <sub>2</sub> Rotameter, SCFM	Open Fully
Load (resistance), ohms	1
H <sub>2</sub> Exhaust pressure, psi	5
O <sub>2</sub> Exhaust pressure, psi	7.5

Procedure

Date/time procedure completed	Initials	Procedure	Comments
8/15/97		1. Read this entire procedure before conducting experiment.	
		2. Place test stand in hood with the front facing the room.	
		3. Place fuel cell stack in the bath container and connect the appropriate fittings.	
		4. Conduct Test Stand Leak Testing Procedure IOP FCP-970705.	

8/16/97  
From Experiment

8/15/97		5. Connect the H <sub>2</sub> , O <sub>2</sub> , and N <sub>2</sub> supply lines to their respective tanks of compressed gas.	
<del>5/16/97</del> Lvd 12/20/97		6. Start the test using the start-up procedure found in Test Stand Start-up/shutdown Procedure IOP FCP-970704.	Proton layer is cooling out Exhaust Plate
		7. Adjust the exhaust valves until the initial exhaust pressures.	See note 1.
		8. Wire the fuel cell in parallel and connected to the 1-ohm load.	
		9. Start recording data on the <u>Stack Experiment Membrane Conditioning</u> form FRM FCP-970804.	The data will be collected every half-hour. See note 2.
		10. Calculate which load is producing the most power. Adjust the potentiometer so the fuel cell is producing the maximum power.	See note 3.
		11. Repeat steps 7 and 8 every half-hour; continue until the fuel cell has operated for 8 hours.	
		12. Conduct the General Stack experiment for one data set.	
		13. Finish the experiment with the shutdown procedure found in Test Stand Start-up/shutdown Procedure IOP FCP-970704.	
		14. Disconnect the supply lines from the inlet lines for the H <sub>2</sub> , O <sub>2</sub> , and N <sub>2</sub> .	
		15. Before leaving make sure that the test stand is in a safe condition.	
		16. Prepare a graph showing volts versus current density	See note 4.



### Notes

1. To acquire the proper exhaust pressure the rotameters should be fully opened and the regulators adjusted greater than the exhaust pressure.
2. The data is recorded by the following method.
  - Record time
  - Record the values of rotameters, hydration temperatures, thermocouples 1-4
  - Record the voltage across the 1-ohm load. Change the load to 5-ohms and wait a few seconds until the voltage settles and record voltage. Repeat for the 10, 25, 35, 50, 65, 80, & 100-ohms loads.
3. From the voltages recorded from step 7 calculate the power produced by the fuel cell by the following equation:

$$P = V^2 / R$$

Adjust the load across the fuel cell to that which is dissipating the most power.

4. Calculate the size of the reaction area of the total stack (cells wired in parallel) in  $\text{cm}^2$  and divide into the current output of the stack. The result will be the amount of current per  $\text{cm}^2$  or current density. Then plot voltage versus current density.

Cell Area cm<sup>2</sup> 55.44000

Appendix B

11:00am Membrane Conditioning: Experiment 08/16/97

resistance	volts	current	current density	power
1	0.037	0.03700	6.674E-04	1.369E-03
5	0.177	0.03540	6.385E-04	6.266E-03
10	0.277	0.02770	4.996E-04	7.673E-03
25	0.430	0.01720	3.102E-04	7.396E-03
35	0.482	0.01377	2.484E-04	6.638E-03
50	0.536	0.01072	1.934E-04	5.746E-03
65	0.569	0.00875	1.579E-04	4.981E-03
80	0.592	0.00740	1.335E-04	4.381E-03
100	0.617	0.00617	1.113E-04	3.807E-03

11:30am

resistance	volts	current	current density	power
1	0.038	0.03800	6.854E-04	1.444E-03
5	0.153	0.03060	5.519E-04	4.682E-03
10	0.247	0.02470	4.455E-04	6.101E-03
25	0.400	0.01600	2.886E-04	6.400E-03
35	0.456	0.01303	2.350E-04	5.941E-03
50	0.512	0.01024	1.847E-04	5.243E-03
65	0.548	0.00843	1.521E-04	4.620E-03
80	0.573	0.00716	1.292E-04	4.104E-03
100	0.600	0.00600	1.082E-04	3.600E-03

12:00pm

resistance	volts	current	current density	power
1	0.035	0.03500	6.313E-04	1.225E-03
5	0.141	0.02820	5.087E-04	3.976E-03
10	0.233	0.02330	4.203E-04	5.429E-03
25	0.383	0.01532	2.763E-04	5.868E-03
35	0.437	0.01249	2.252E-04	5.456E-03
50	0.496	0.00992	1.789E-04	4.920E-03
65	0.534	0.00822	1.482E-04	4.387E-03
80	0.562	0.00703	1.267E-04	3.948E-03
100	0.590	0.00590	1.064E-04	3.481E-03

12:30pm

resistance	volts	current	current density	power
1	0.042	0.04200	7.576E-04	1.764E-03
5	0.188	0.03760	6.782E-04	7.069E-03
10	0.280	0.02800	5.051E-04	7.840E-03
25	0.436	0.01744	3.146E-04	7.604E-03
35	0.482	0.01377	2.484E-04	6.638E-03
50	0.540	0.01080	1.948E-04	5.832E-03
65	0.570	0.00877	1.582E-04	4.998E-03
80	0.596	0.00745	1.344E-04	4.440E-03
100	0.617	0.00617	1.113E-04	3.807E-03

1:30pm

resistance	volts	current	current density	power
1	0.051	0.05100	9.199E-04	2.601E-03
5	0.212	0.04240	7.648E-04	8.989E-03
10	0.320	0.03200	5.772E-04	1.024E-02
25	0.464	0.01856	3.348E-04	8.612E-03
35	0.514	0.01469	2.649E-04	7.548E-03
50	0.562	0.01124	2.027E-04	6.317E-03
65	0.593	0.00912	1.646E-04	5.410E-03
80	0.616	0.00770	1.389E-04	4.743E-03
100	0.638	0.00638	1.151E-04	4.070E-03

2:00pm

resistance	volts	current	current density	power
1	0.052	0.05200	9.380E-04	2.704E-03
5	0.220	0.04400	7.937E-04	9.680E-03
10	0.325	0.03250	5.862E-04	1.056E-02
25	0.472	0.01888	3.405E-04	8.911E-03
35	0.516	0.01474	2.659E-04	7.607E-03
50	0.561	0.01122	2.024E-04	6.294E-03
65	0.561	0.00863	1.557E-04	4.842E-03
80	0.590	0.00738	1.330E-04	4.351E-03
100	0.612	0.00612	1.104E-04	3.745E-03

2:30pm

resistance	volts	current	current density	power
1	0.059	0.05900	1.064E-03	3.481E-03
5	0.211	0.04220	7.612E-04	8.904E-03
10	0.315	0.03150	5.682E-04	9.923E-03
25	0.463	0.01852	3.341E-04	8.575E-03
35	0.515	0.01471	2.654E-04	7.578E-03
50	0.560	0.01120	2.020E-04	6.272E-03
65	0.593	0.00912	1.646E-04	5.410E-03
80	0.616	0.00770	1.389E-04	4.743E-03
100	0.636	0.00636	1.147E-04	4.045E-03

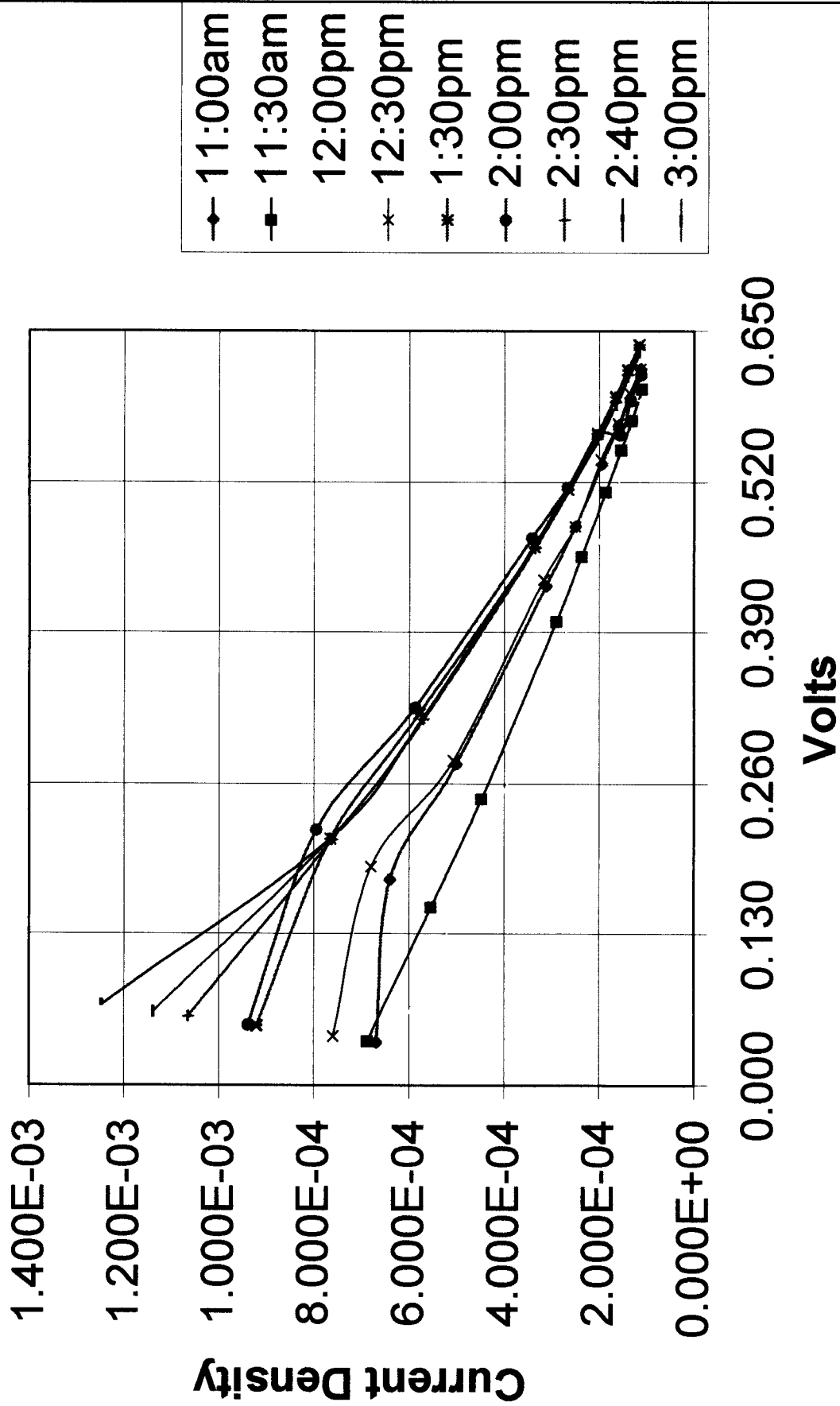
2:40pm

resistance	volts	current	current density	power
1	0.069	0.06900	1.245E-03	4.761E-03
5	0.212	0.04240	7.648E-04	8.989E-03
10	0.316	0.03160	5.700E-04	9.986E-03
25	0.463	0.01852	3.341E-04	8.575E-03
35	0.512	0.01463	2.639E-04	7.490E-03
50	0.556	0.01112	2.006E-04	6.183E-03
65	0.586	0.00902	1.626E-04	5.283E-03
80	0.610	0.00763	1.375E-04	4.651E-03

3:00pm

resistance	volts	current	current density	power
100	0.630	0.00630	1.136E-04	3.969E-03
1	0.063	0.06300	1.136E-03	3.969E-03
5	0.212	0.04240	7.648E-04	8.989E-03
10	0.316	0.03160	5.700E-04	9.986E-03
25	0.465	0.01860	3.355E-04	8.649E-03
35	0.515	0.01471	2.654E-04	7.578E-03
50	0.558	0.01116	2.013E-04	6.227E-03
65	0.587	0.00903	1.629E-04	5.301E-03
80	0.611	0.00764	1.378E-04	4.667E-03
100	0.632	0.00632	1.140E-04	3.994E-03

# Membrane Performance-Current Density



Hand Calculations

Contents

Calculations of Flow Rates for Hydrogen and Oxygen.

Calculations for Amount of TBOH Used.

## Calculations of Flow Rates for Hydrogen and Oxygen

GIVEN: 1 AMP/CM<sup>2</sup>  
0.6 VOLTS

POWER:  $P = VI = (0.6)(1) = 0.6 \text{ WATTS/CM}^2 = \frac{6 \times 10^{-4} \text{ KJ}}{\text{S} \cdot \text{CM}^2}$

$$\dot{n} = \frac{\text{POWER } \rho}{\Delta G} = \frac{-6 \times 10^{-4} \frac{\text{KJ}}{\text{S} \cdot \text{CM}^2}}{-237 \frac{\text{KJ}}{\text{mol H}_2}} = \underline{\underline{2.53 \times 10^{-6} \frac{\text{mol H}_2}{\text{S} \cdot \text{CM}^2}}}$$

FOR H<sub>2</sub>:

$$\dot{V} = \frac{\dot{n} RT}{P} = \left( 2.53 \times 10^{-6} \frac{\text{mol H}_2}{\text{S} \cdot \text{CM}^2} \right) \left( 8.314 \frac{\text{J Pa m}^3}{\text{J mol} \cdot \text{K}} \right) (293.15 \text{ K}) \left( \frac{1}{101300 \text{ Pa}} \right) = \underline{\underline{6.09 \times 10^{-8} \frac{\text{m}^3 \text{ H}_2}{\text{S} \cdot \text{CM}^2}}}$$

electro-cataly.

\*  $PV = \text{WORK} = E = J = \text{Pa} \cdot \text{m}^3$

CONVERT  $\dot{V}$  TO SCFM

$$\dot{V} = \left( 6.09 \times 10^{-8} \frac{\text{m}^3 \text{ H}_2}{\text{S} \cdot \text{CM}^2 \text{ electro. cat.}} \right) \left( \frac{1 \text{ ft}}{0.3048 \text{ m}} \right)^3 \left( \frac{60 \text{ S}}{1 \text{ MIN}} \right) \left( \frac{30.48 \text{ CM}}{1 \text{ ft}} \right)^2$$

$$\dot{V} = \underline{\underline{0.11995 \frac{\text{ft}^3 \text{ H}_2}{\text{MIN ft}^2 \text{ electro. cat.}}}} \quad \checkmark$$

FOR O<sub>2</sub>:

$$\frac{1}{2} \text{O}_2 = 1 \text{ mol H}_2$$

$$\dot{V} = (1.5) \left( 0.11995 \frac{\text{ft}^3 \text{ H}_2}{\text{MIN ft}^2 \text{ electro. cat.}} \right)$$

$$\dot{V} = \underline{\underline{59.975 \times 10^{-3} \frac{\text{ft}^3 \text{ O}_2}{\text{MIN ft}^2 \text{ electro. cat.}}}} \quad \checkmark$$

### Calculations for Amount of TBOH Used

Given: for a 1-1 molar ratio of Nafion 5% by wt. solution and TBOH.

Amount of Nafion solution weighed = 1.33g

$\therefore$  Amount of Nafion =  $(0.05 \times 1.33)g = 0.0665g$  of Nafion

Molecular wt of Nafion = 1100g Nafion

$\therefore 0.0665g \text{ Nafion} \times \left( \frac{1 \text{ mol Nafion}}{1100g} \right) = \underline{\underline{6.045 \times 10^{-5} \text{ mol Nafion}}}$

For 50% excess: Need 1.5 amount of TBOH to Nafion (1:1)

$\therefore (1.5)(6.045 \times 10^{-5} \text{ mol Nafion}) = \underline{\underline{9.0682 \times 10^{-5} \text{ TBOH}}}$

molecular wt of TBOH = 259.48g

Amount of TBOH 50% in excess needed in grams:

$(9.0682 \times 10^{-5} \text{ mol TBOH}) \left( \frac{259.48g \text{ TBOH}}{1 \text{ mol}} \right) = \underline{\underline{2.353 \times 10^{-2} g \text{ TBOH}}}$

Volume of TBOH 50% in excess needed:

$(2.353 \times 10^{-2} g \text{ TBOH}) \left( \frac{1 \text{ ml}}{0.001g} \right) = \underline{\underline{23.53 \text{ ml TBOH } \checkmark}}$   
(50% excess)



Appendix D

Specifics for Certain Recommendations

Contents

Wiring Harness

- Perform conductivity test for circuit efficiency.

General

- There are many possibilities to include other departments to accomplish the recommendations of this report.

### Wiring Harness

- Perform conductivity test for circuit efficiency.

With the electrodes installed into the plates place a sheet of copper in place of the membrane. Apply a voltage through the copper plate, electrode and through the external connection. Measure the voltage drop across the electrode and ~~the~~ the connection from the electrode and external contact. {Find if the voltage is increased is there a point where the thermal effects on the electrical path cause a change in resistance that limits the potential of the fuel cells.}

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### General

- There are many possibilities to include other departments to accomplish the recommendations of this report.
1. The material properties of some of the components of the prototype need to be further investigated which could use the aid of Material Science Students.
  2. A new and improve wiring harness with the capability to change the parameters of the test and record the results could use aid of Electrical Engineers. The EE could also be used in the design of the overall safety system if it involves one switch to control solenoids that shuts down the fuel cell and fuel gases.
  3. Technical Communications for maintaining the Web Site and administrating continuity of project documentation.