

# Effects of Moisture Diffusion in Sandwich Composites

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University of Washington  
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## Outline

- I.** Brief summary of a UW numerical study funded by Boeing in 2003
  - II.** Experimental studies at UW, 2008-09
  - III.** Newly-funded JAMS-AMTAS project, initiated September 2015
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  - Fourier heat conduction equation → used to predict steady-state through-thickness temperature profiles
  - Clapeyron equations → used to predict dew point of water vapor in core (if current temperature < dew point, condensation occurs)
  - Certain properties of core region estimated using rule-of-mixtures
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## Overall Conclusions:

- Core humidity levels will increase with time...only question is time required
  - Under realistic service conditions liquid water does not accumulate within core region of pristine structures due strictly to diffusion...however
  - (For transport aircraft flight profiles) humidity increase implies water vapor will condense-freeze-thaw-evaporate during ascent-cruise-descent cycles
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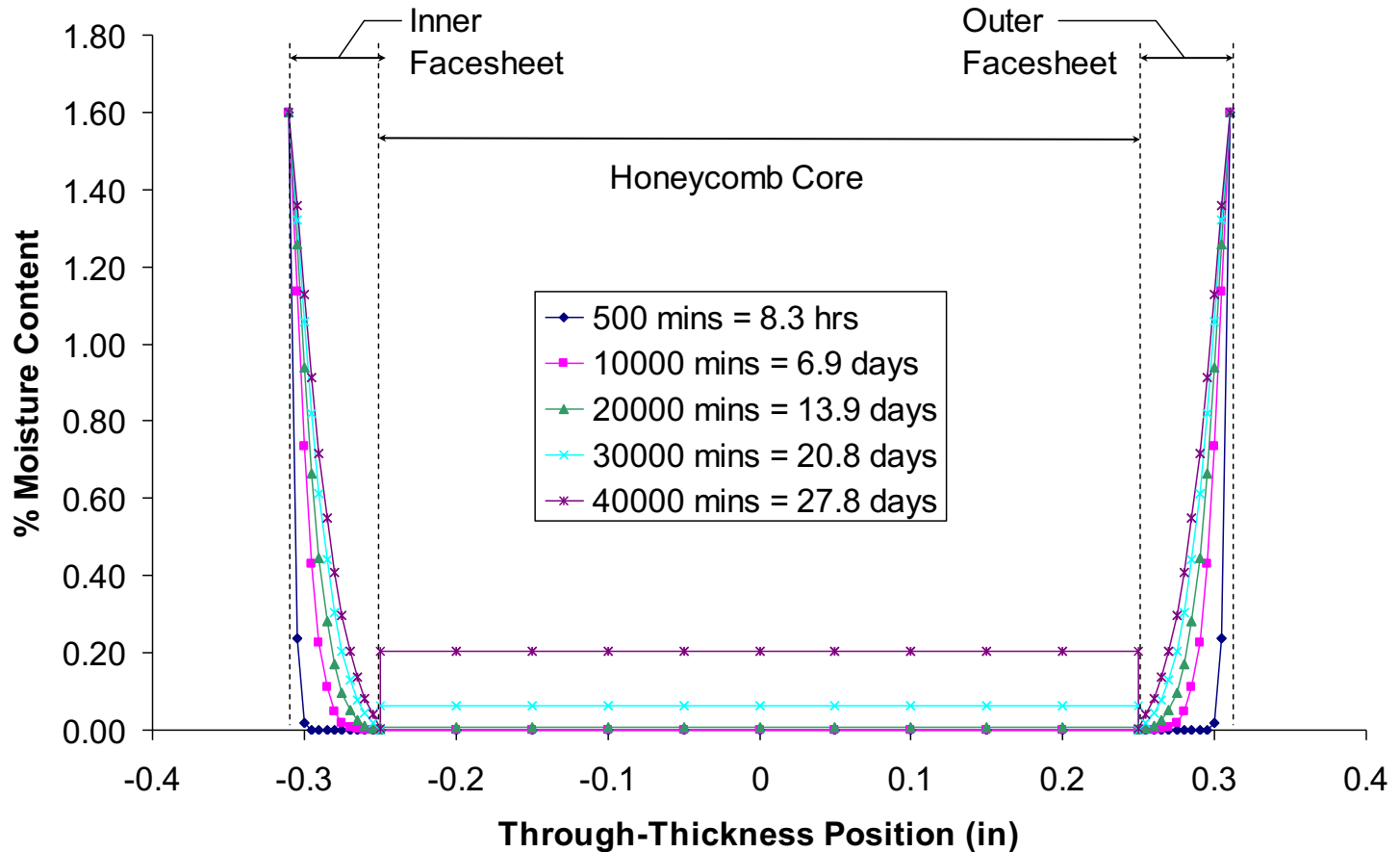
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# Predicting Moisture Diffusion

*Typical Result: Constant Temperatures and Humidity*

12-ply Gr/Ep inner and outer facesheets  
 0.50 in honeycomb core with 0.20 in cell size  
 T=90F (both faces; constant)  
 RH = 80% (both faces, constant)





# Predicting Moisture Diffusion

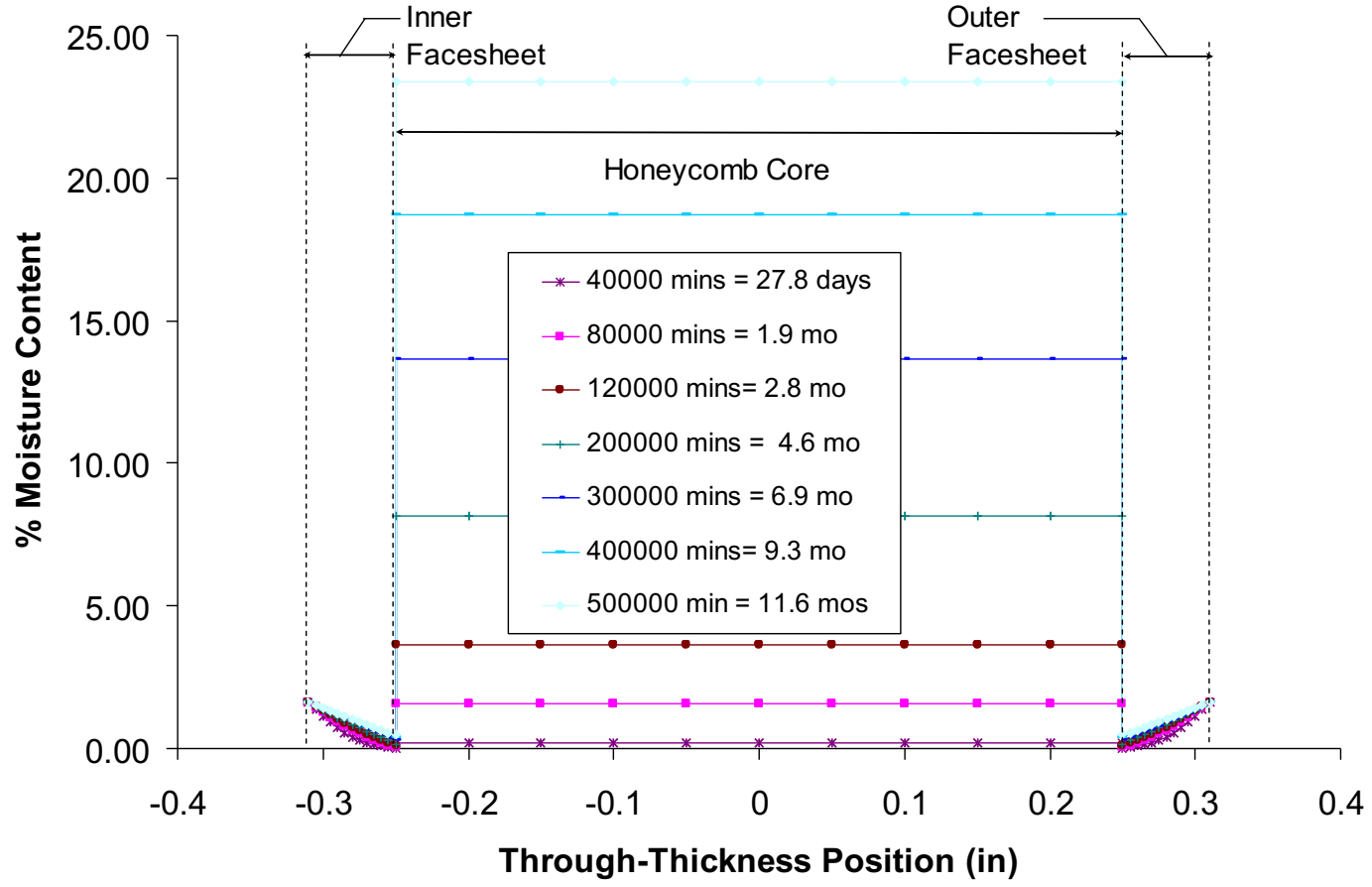
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# Numerical UW Study Funded by Boeing in 2003

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Although reasonable predictions were obtained using program MOIST, no experimental measurements were available to validate analysis

The potential structural application of sandwich composites envisioned by Boeing engineers (in 2003) were not pursued, funding was discontinued, and the UW study ended.

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Objectives:

Measure relative humidity in core region of a flat sandwich panel exposed to constant external temperature and humidity on both sides

Compare measurements with MOIST predictions

Sandwich panel internally instrumented with:

- 2 type K thermocouples
- 2 Ohmic Instruments Model HC-610 capacitive humidity sensors:
  - 5-95 %RH
  - -40 to 185°F operating range

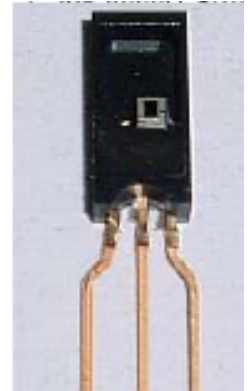
Test begun on 5 Aug 2008:

- Temperature set @ 40°C (104°F)
- Humidity level 55%RH
- Data recorded every 30 mins (using Labview)

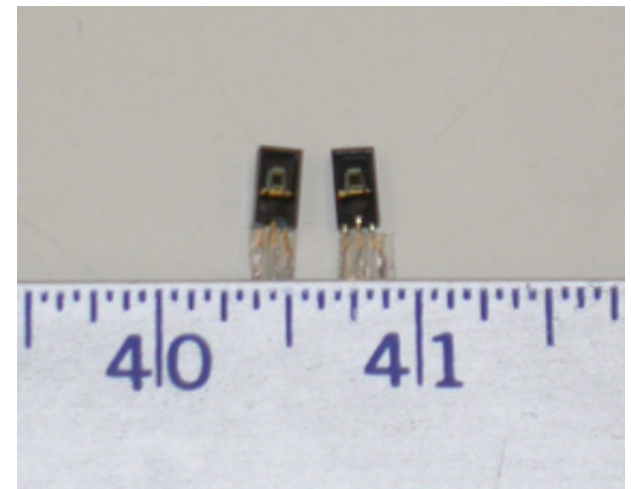
HC-610 Thermoset polymer capacitive humidity sensor. Hybrid electronics. Linear output. Range 5 to 95 %RH 2%. Temp. - 40 to 185 °F. Supply voltage 4.0 - 5.8 VDC

PDF Data

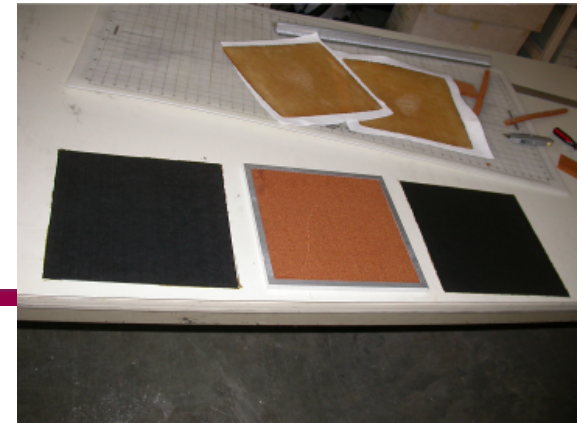
PDF Man/Instructions



[www.ohmicinstruments.com/](http://www.ohmicinstruments.com/)



# Test Panel Fabrication

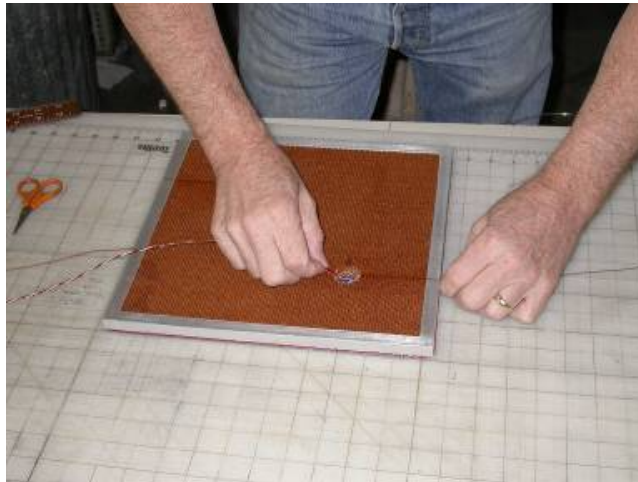


- Type 410 Nomex honeycomb core
- $[0/45/90/-45]_s$  Gr/Ep facesheets
- Core sized to fit within aluminum frame to insure 1-D, through-thickness diffusion
- First facesheet bonded to one side of panel using thin-film adhesive
- Pocket for embedded humidity sensors and thermocouples milled in core



# Test Panel Fabrication

- Leadwires inserted through honeycomb and aluminum frame

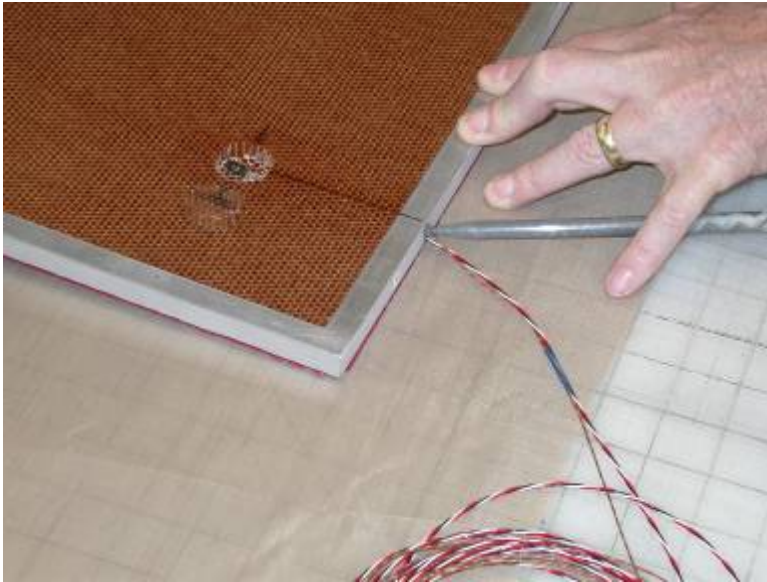


- Initial installation of embedded sensors



# Test Panel Fabrication

- Leadwire passage in aluminum frame sealed with epoxy



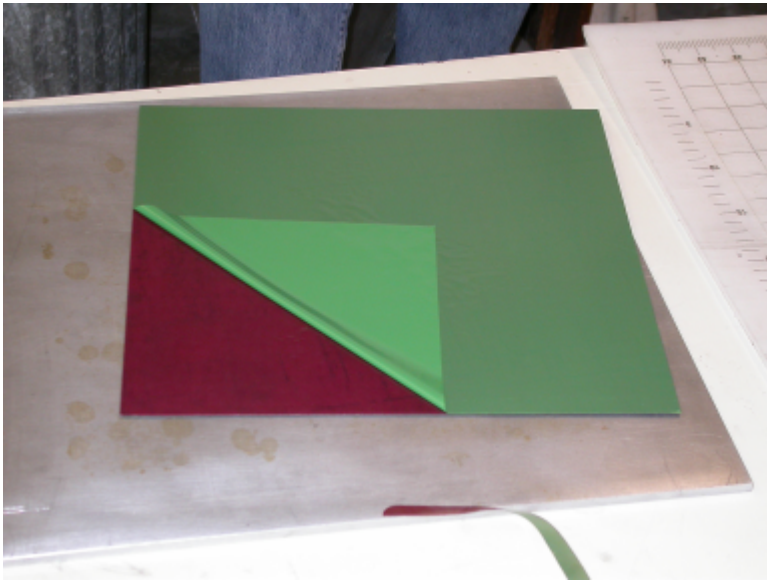
- Honeycomb 'caps' placed over instrumented sites





# Test Panel Fabrication

- Second facesheet bonded to panel using thin-film adhesive...

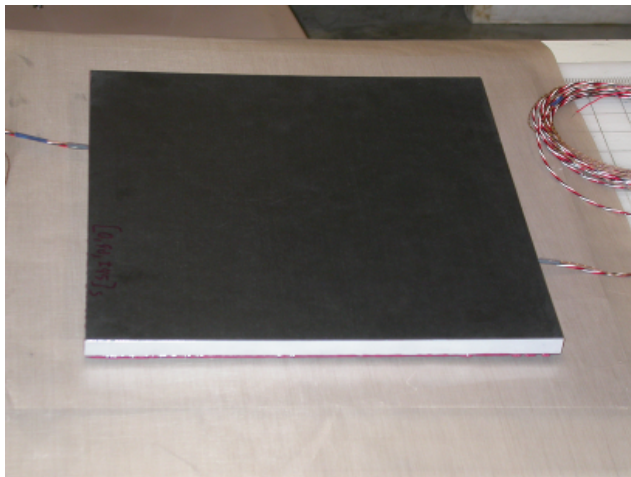


...and hot press



# Test Panel Fabrication

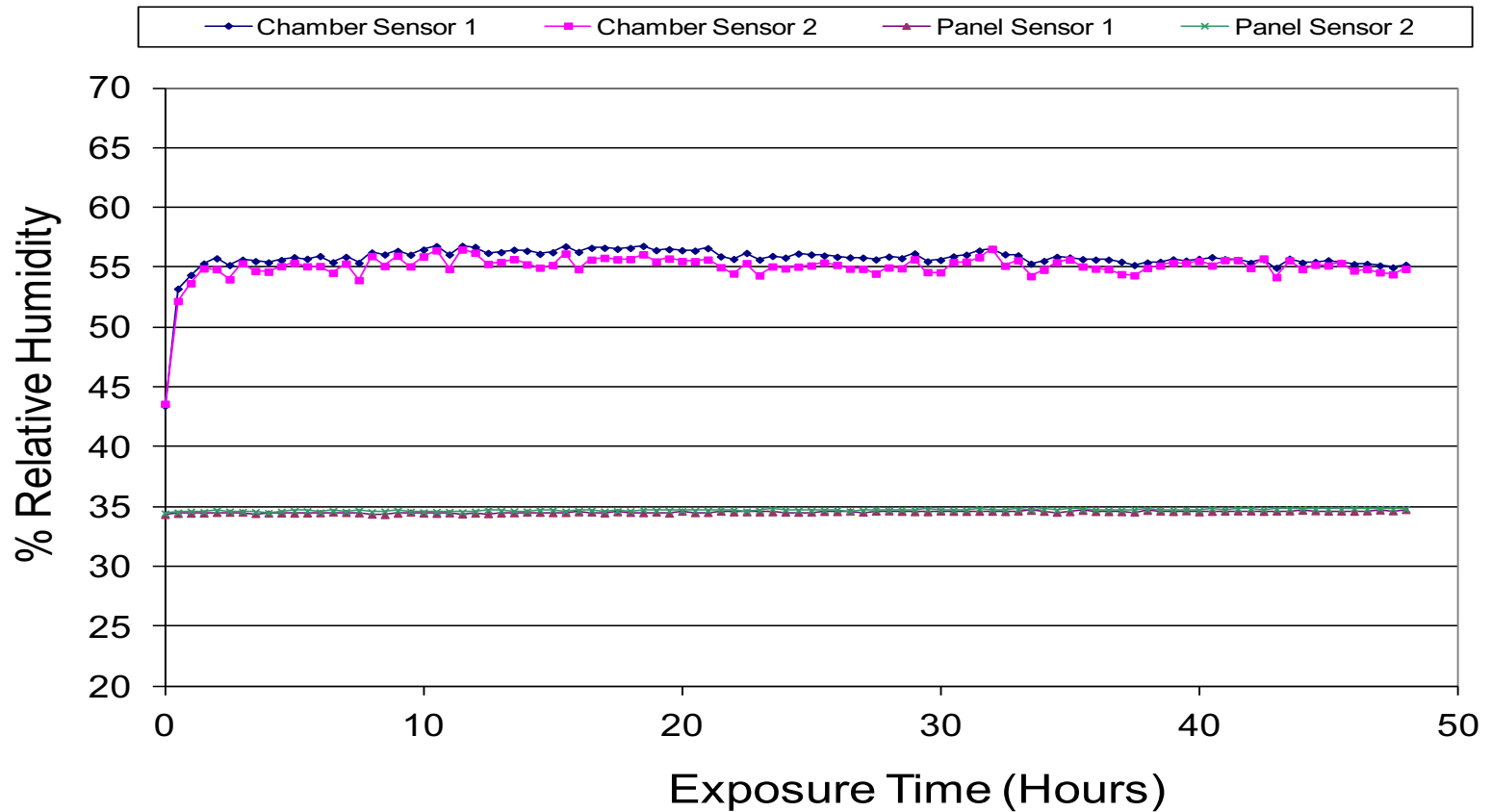
- Completed panel mounted in test chamber; exposure began on 5 Aug 2008
- Initial measurements (40°C = 104°F):
  - Panel hum sensor 1: 25.0 %RH
  - Panel hum sensor 2: 23.4 %RH
  - (...higher than anticipated in '03...)



# Typical Measurements

Humidity data from 7:50am 3 Nov to  
7:50am 5 Nov

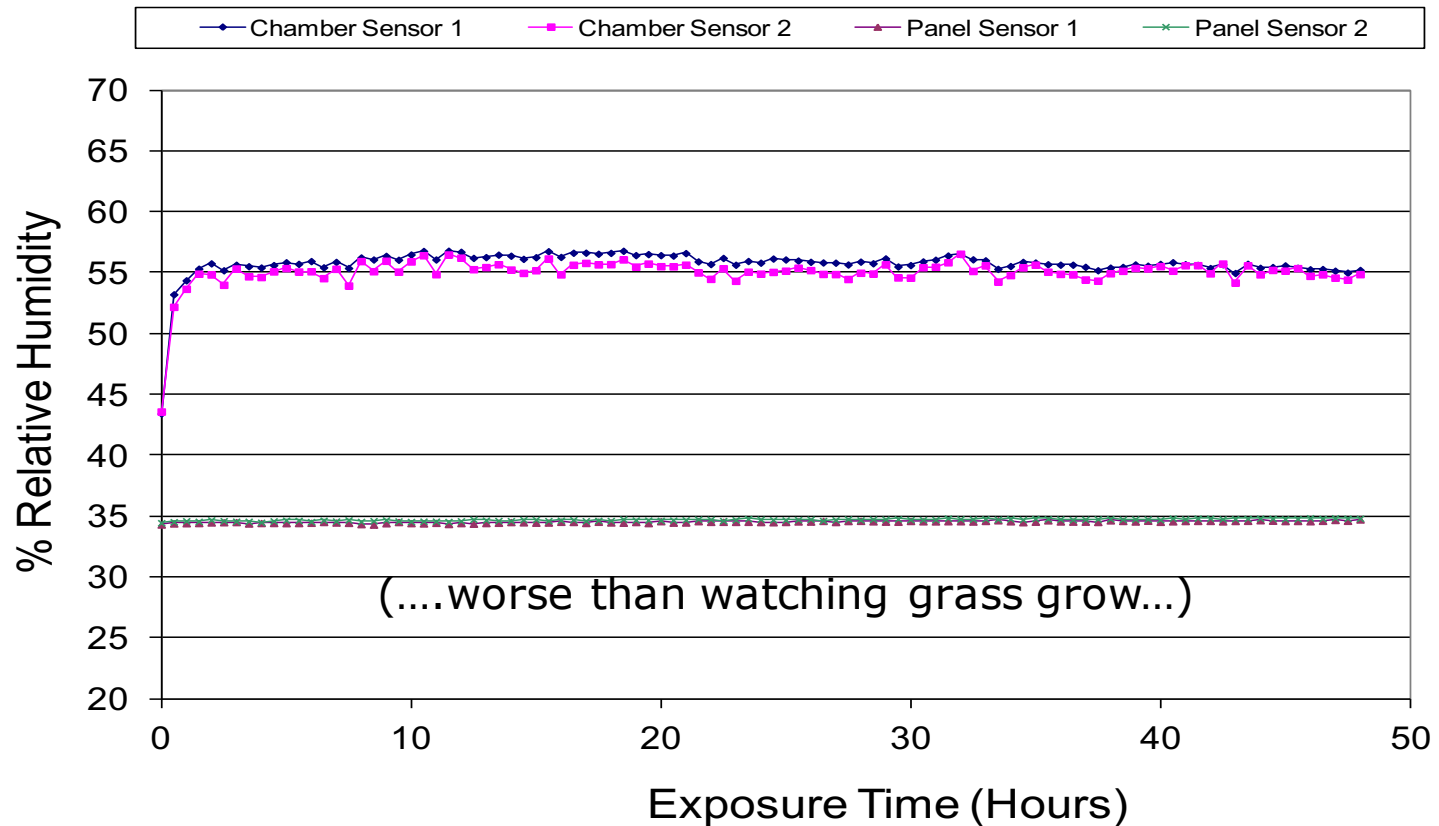
(48 hr period, about 3 months after test  
initiated)



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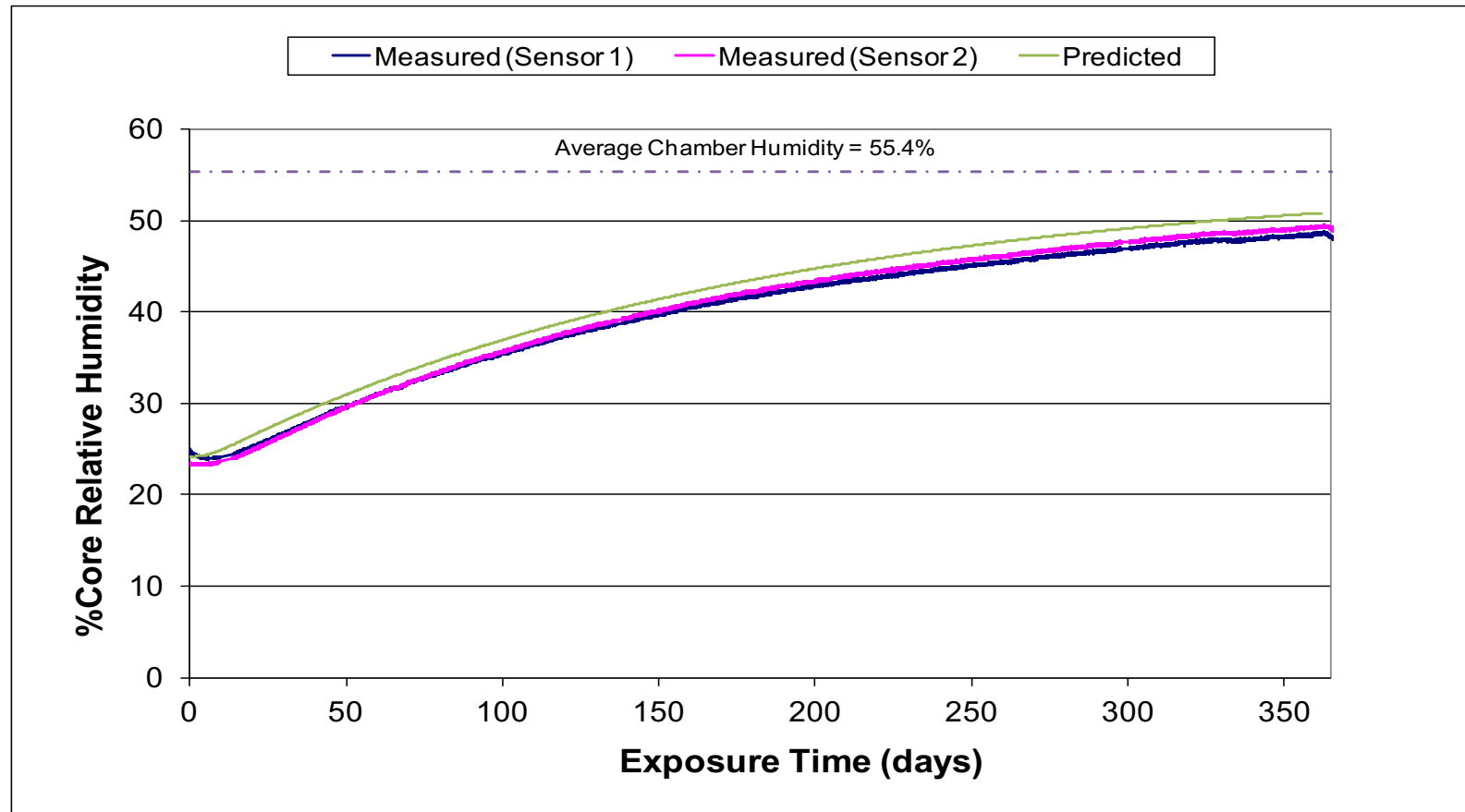
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# Measurement vs Prediction

*Obtained between 5 Aug '08 to 4 Aug '09 = 365 days*



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Overall objective: Determine if condense-freeze-thaw-  
evaporate cycle within core region cycle is  
detrimental...measure:

- Change in bending stiffness,  $EI_{\text{eff}}$  (measure using 4-pt bend test)
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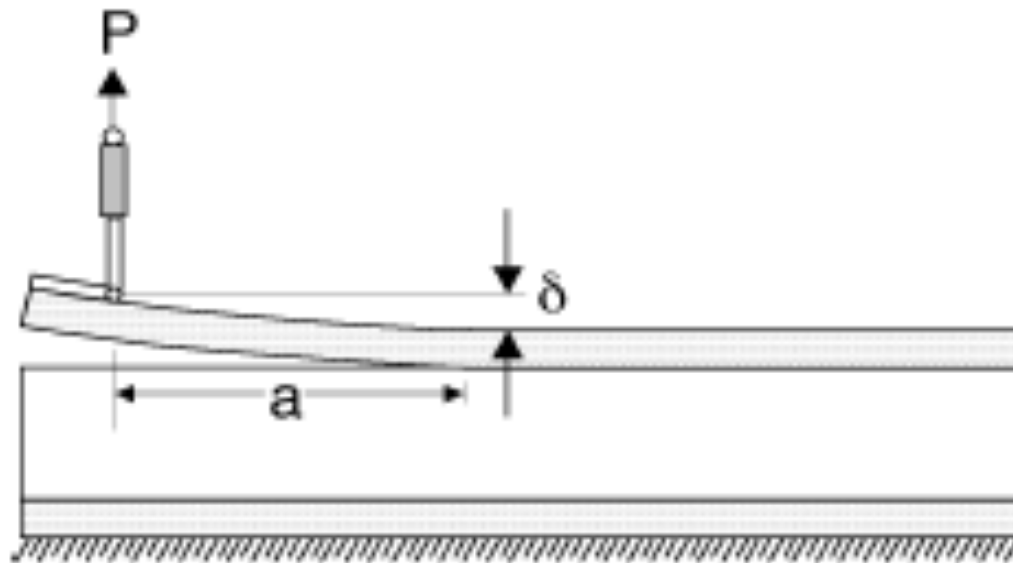
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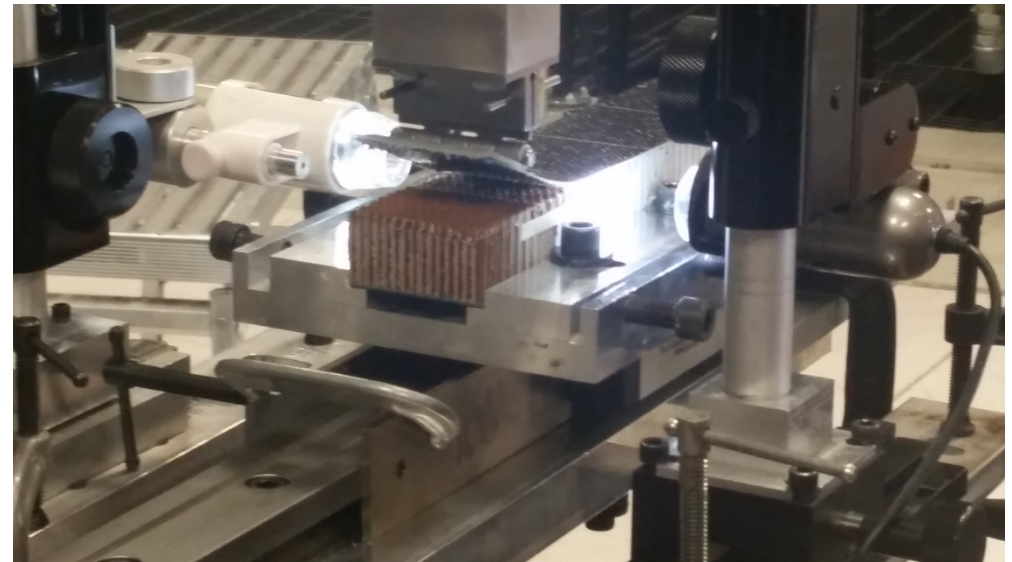
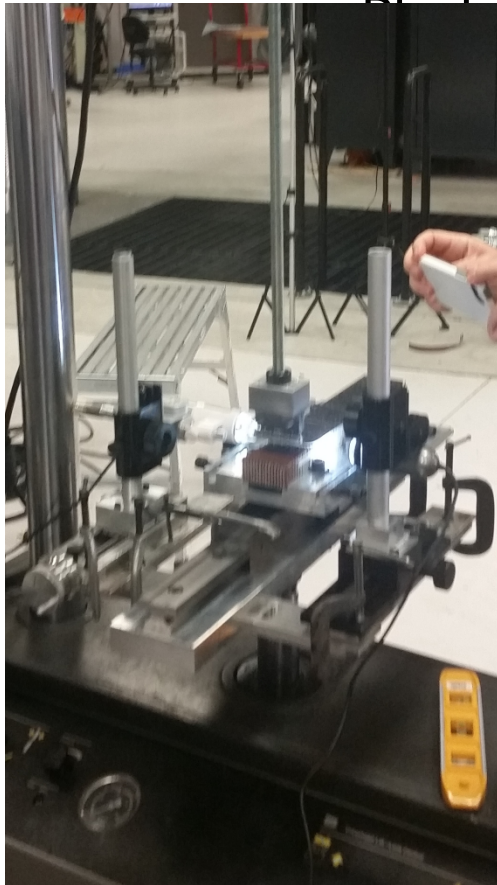
Schematic of experimental arrangement to measure  $G_I$  for sandwich panels (under development by CMH-17 working group)



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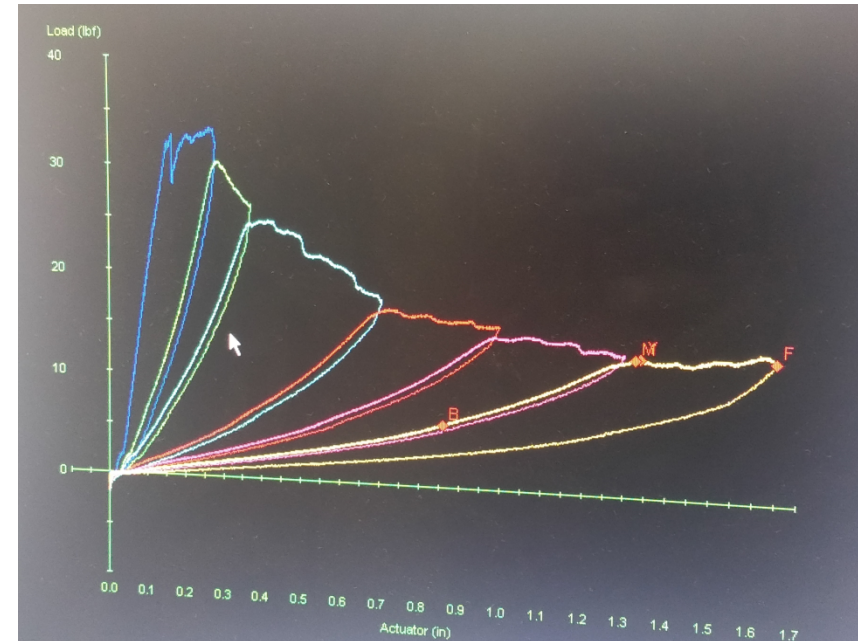
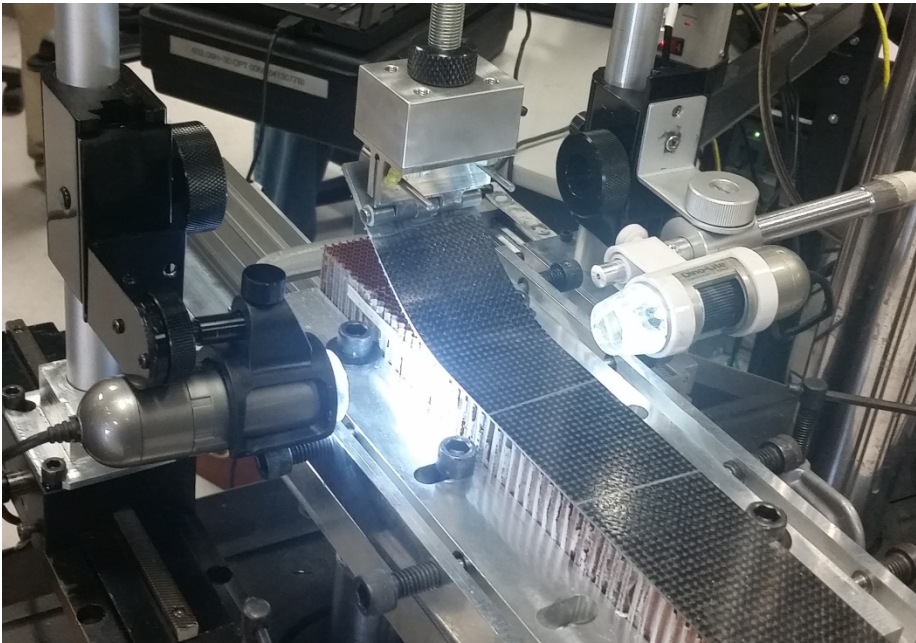
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Photographs of test setup at NIAR



# Effects of Moisture Diffusion in Sandwich Composites

Photos of test setup at NIAR





# Effects of Moisture Diffusion in Sandwich Composites

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Thank You!

Comments/Questions/Suggestion  
s?

# Backup Slides

# Effects of Moisture Diffusion in Sandwich Composites



American Autoclave featuring 42 in dia x 96 in working chamber

# Effects of Moisture Diffusion in Sandwich Composites



Blue-M Model POM-246F  
Lab Oven



Wabash Model G50H-24-  
BCLX  
50-ton hot press

# Effects of Moisture Diffusion in Sandwich Composites



Cincinnati Sub-Zero "Tundra"  
Environmental Conditioning Chamber

# Effects of Moisture Diffusion in Sandwich Composites



Thermotron Model S.12 Temperature Chamber

# Effects of Moisture Diffusion in Sandwich Composites

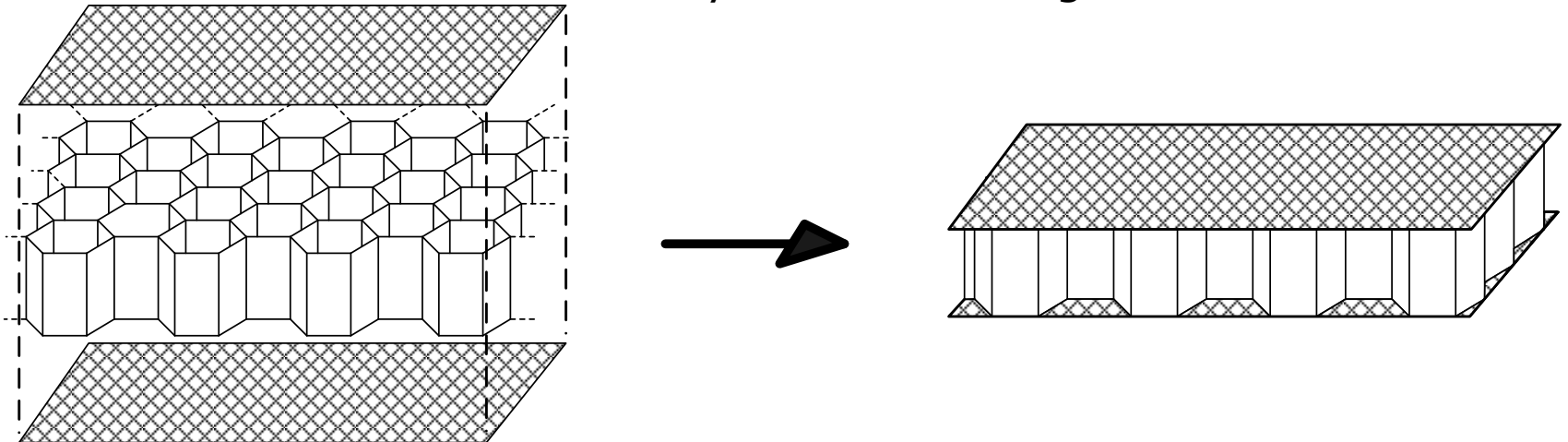


Instron Model 8511 hydraulic test frame

# Synopsis: Numerical UW Study Funded by Boeing in 2003

## Assumptions:

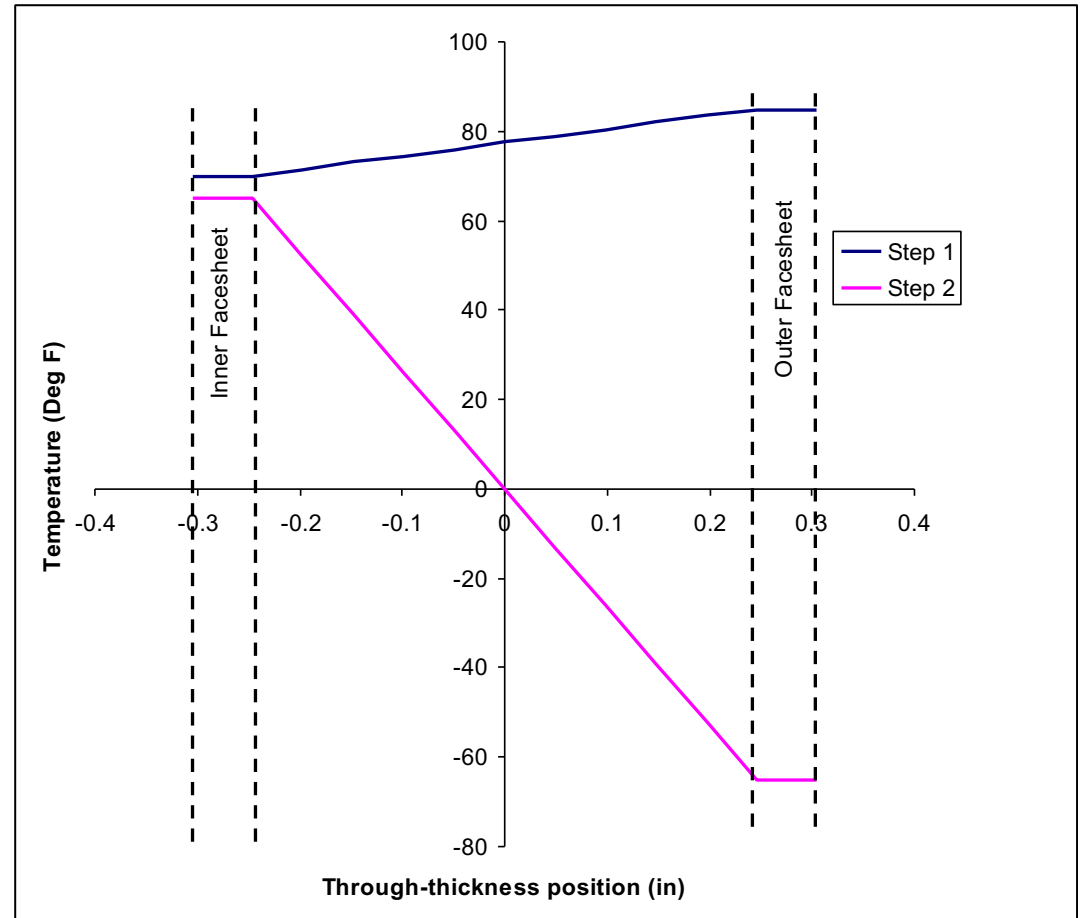
- 'Pristine' (undamaged) sandwich structure; moisture ingress solely due to diffusion
- Core = Nomex honeycomb
- Initial moisture content = 0% . This implies:
  - Initial moisture content of composite face sheets = 0%
  - Initial relative humidity within core region = 0%



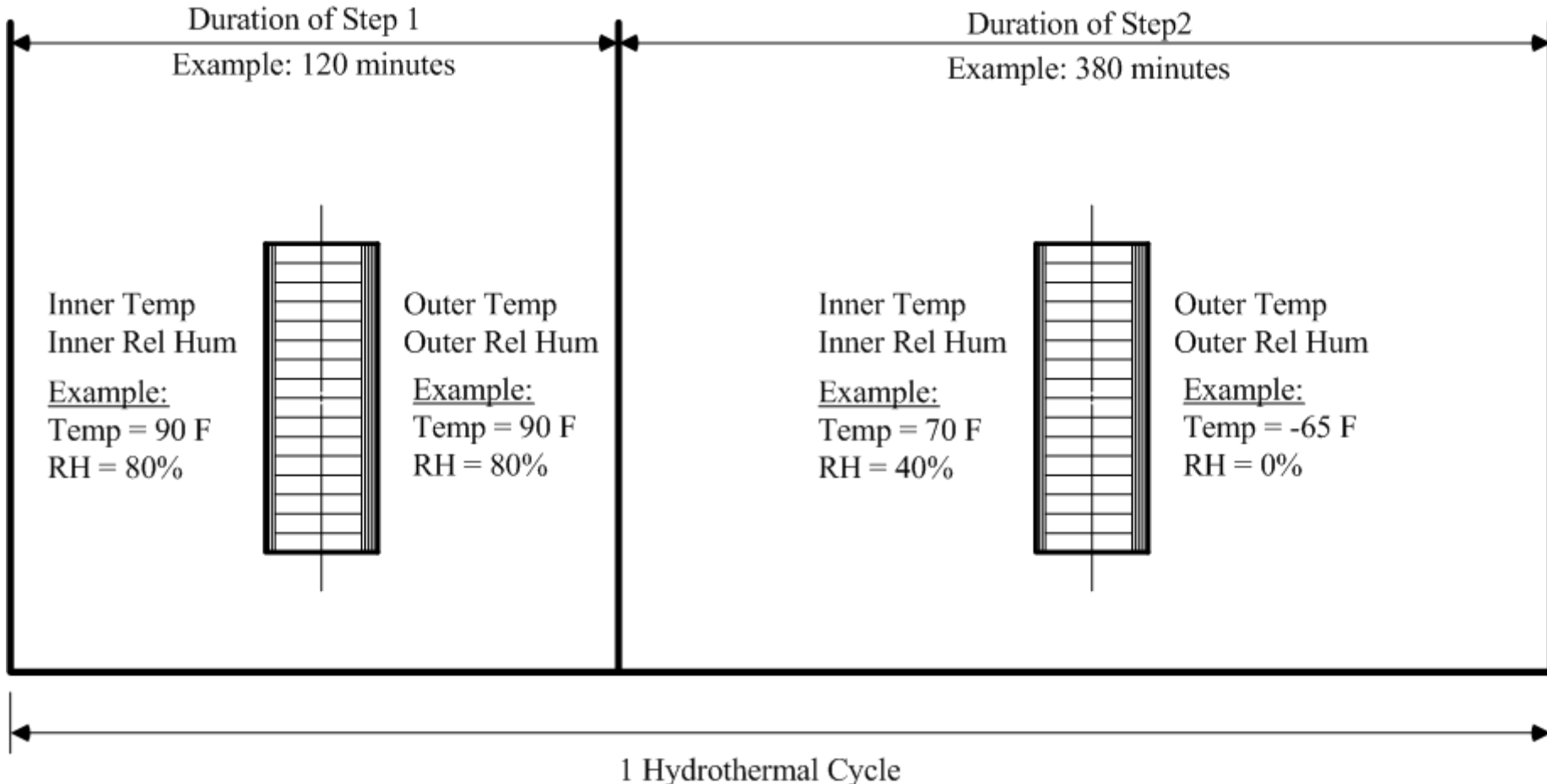


# Typical Predicted Steady-State Temperature Profiles

- 12-ply Gr-Ep facesheets (0.060 in thick)
- Nomex honeycomb core (0.50 in thick)
- Step 1:  
Inside temp = 70F  
Outside temp = 85F
- Step 2:  
Inside temp = 65F  
Outside temp = -65F



# Definition of a Cycle



# Typical Analysis

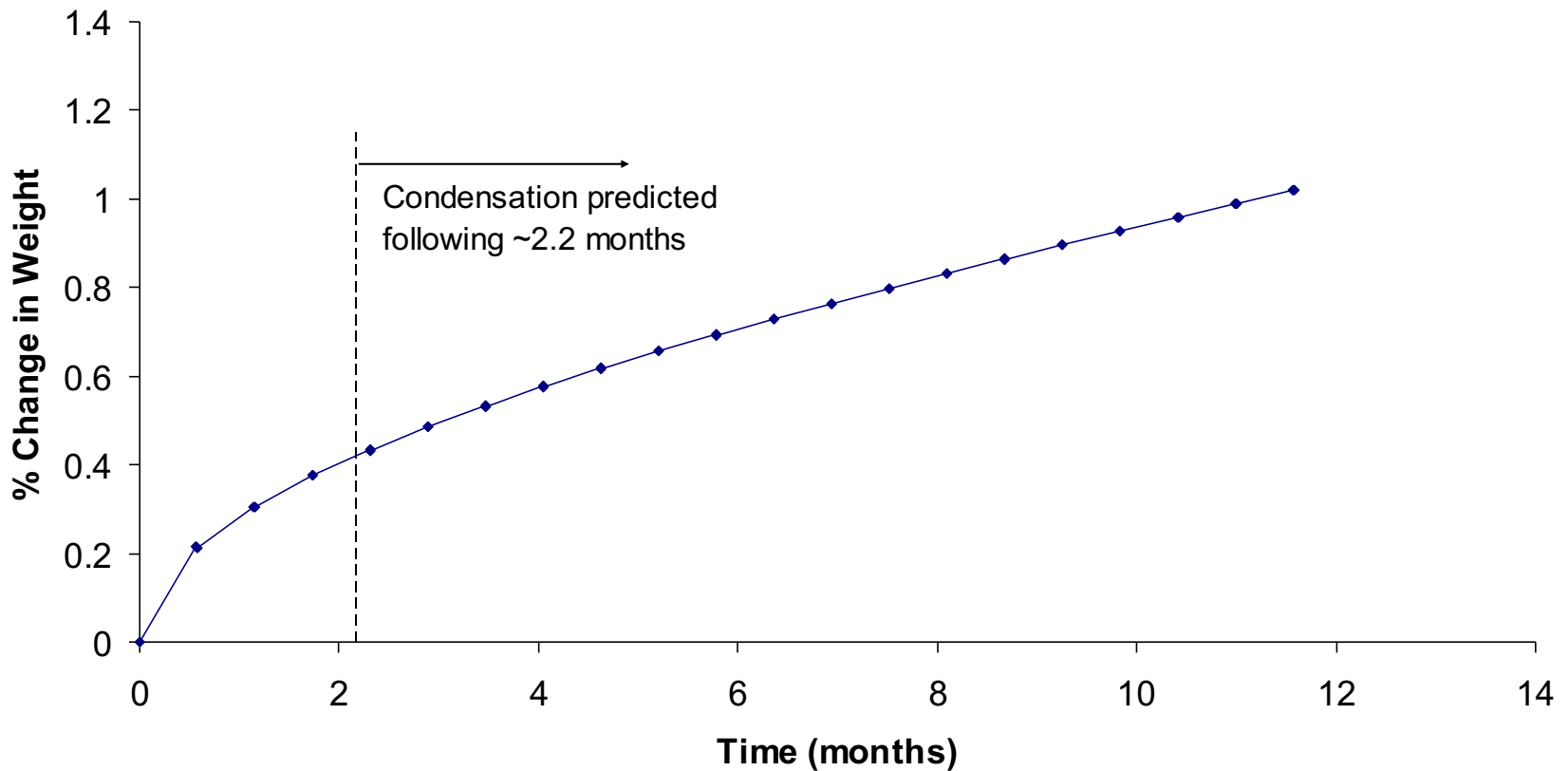
## *Cyclic Changes in Temperature and Humidity*

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- Step 1:  
Duration: 120 minutes  
Inside: temp = 90F; RH = 80%  
Outside: temp = 90F; RH = 80%
- Step 2:  
Duration: 380 minutes  
Inside: temp = 70F; RH = 40%  
Outside: temp = -65F; RH = 0%
- (Total cycle time = 500 minutes = 8.3 hrs)
- 12-ply Gr-Ep facesheets (0.060 in thick)
- Nomex honeycomb core (0.50 in thick)
- Initial moisture content assumed = 0%

# Typical Analysis

## *Cyclic Changes in Temperature and Humidity*



# Typical Analysis

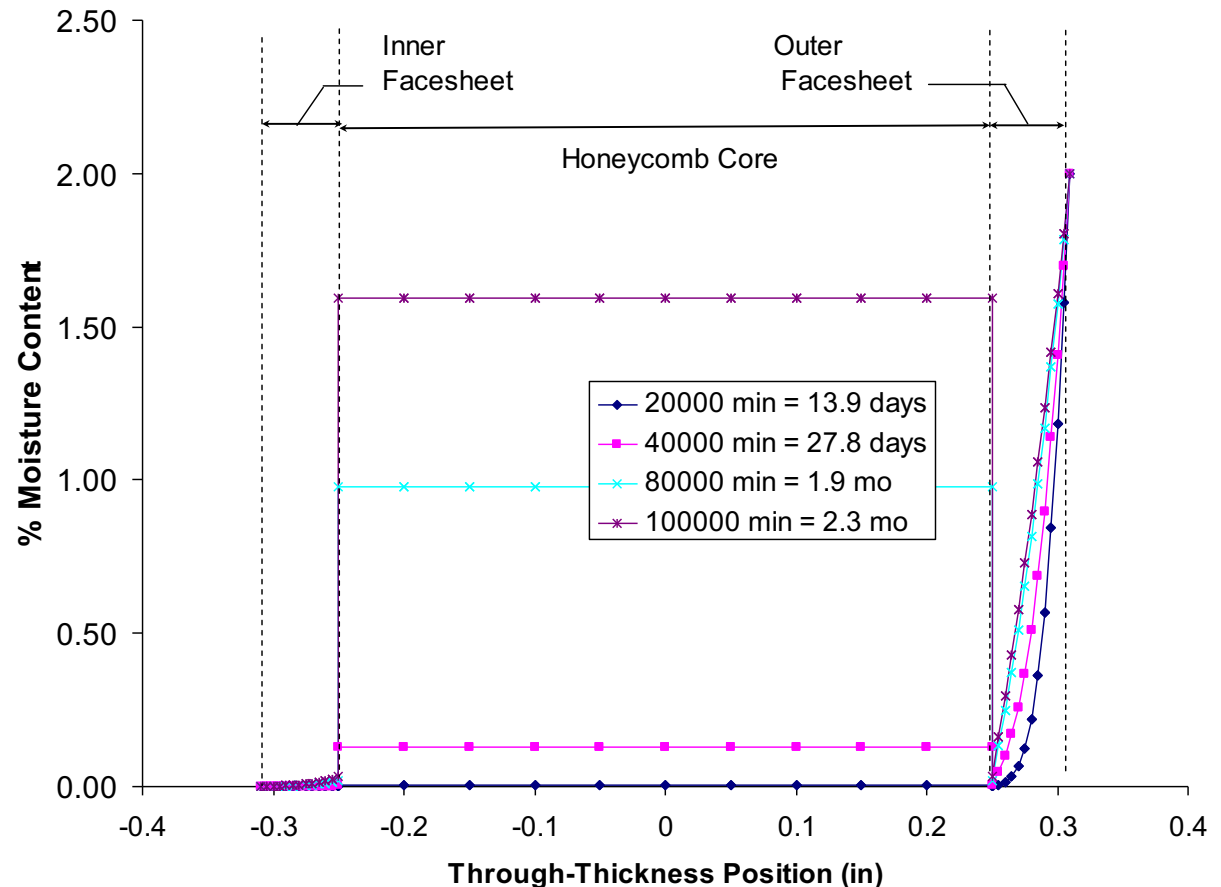
## Constant Temperatures, Non-uniform Humidity

12-ply Gr/Ep  
 inner and  
 outer  
 facesheets

0.50 in  
 honeycomb  
 core with  
 0.20 in cell  
 size

Outer: T=90F;  
 RH = 100%  
 (constant)

Inner: T=90F;  
 RH = 0%  
 (constant)



# Temperature predictions

- Through-thickness temperature distribution assumed to be governed by the Fourier heat conduction equation:

$\partial Q / \partial t =$  heat transfer rate

$K_z =$  thermal conductivity ( $z$  - direction)

where:  
 $A = \text{area} - K_z A \frac{\partial T}{\partial z}$

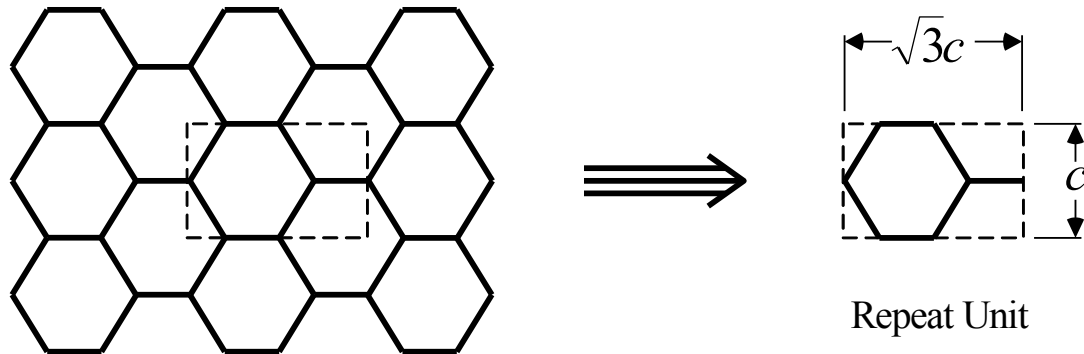
$T =$  temperature

$t =$  time

- Material properties allowed to vary through thickness; heat conduction equation solved numerically using finite-differences

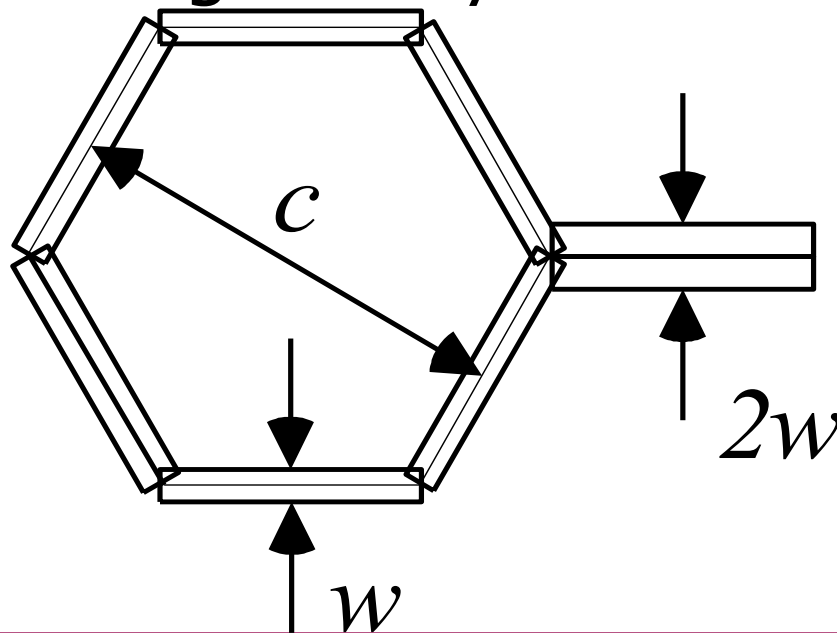
# Core Thermal Conductivity

- $K_{core}$  estimated using rule-of-mixture approach
- Volume fractions of air and paper within the core calculated using hexagonal repeat unit



# Core Thermal Conductivity

- Given the cell size ( $c$ ), paper ribbon thickness ( $w$ ), and core thickness ( $t$ ), it can be shown that the volume fractions are given by:



$$V_{air} = \frac{(3c - 8w)}{3c}$$

$$V_{paper} = \frac{8w}{3c}$$



# Core Thermal Conductivity

Example: 
$$K_{core} = (V_{air})(K_{air}) + (V_{paper})(K_{paper})$$

Honeycomb core with 0.20 in cell size, produced using 2-mil thick DuPont Type 410 Nomex paper:

$$K_{paper} = 0.715 \text{ BTU-in/hr-ft}^2\text{-}^\circ\text{R}$$

$$K_{air} = 0.166 \text{ BTU-in/hr-ft}^2\text{-}^\circ\text{R}$$

Calculated quantities:

$$V_{paper} = 0.027$$

$$V_{air} = 0.973$$

$$K_{core} = 0.181 \text{ BTU-in/hr-ft}^2\text{-}^\circ\text{R}$$

\* Nomex properties: <http://www.matweb.com>

Air properties: *Marks' Standard Handbook for Mechanical Engineers*, 8<sup>th</sup> Ed (1978)

# Typical Properties

Material	Thermal Conductivity, K (BTU-in/hr-ft <sup>2</sup> -°R)	Thickness (in)
Graphite/Epoxy	4.0*	0.005 (ply)
Honeycomb Core	0.181	0.50

\* Note: Typical through-thickness K for Gr/Ep is listed; in-plane K values typically > 400 BTU-in/hr-ft<sup>2</sup>-°R

# Predicting Moisture Diffusion

- Through-thickness (1-D) diffusion of moisture assumed to be governed by Fick's first and second laws:

$$\phi = D_z \frac{\partial c}{\partial z} \qquad \frac{\partial c}{\partial t} = \frac{\partial}{\partial z} \left[ D_z \frac{\partial c}{\partial z} \right]$$

$\phi$  = rate of diffusion ("moisture flux") : units = mass/(area \* time)

$c$  = concentration : units = (mass/volume)

$D_z$  = diffusivity : units = area/time

$z$  = direction of diffusion : unit = length

$t$  = time

# Predicting Moisture Diffusion

- From an experimental point of view it is easier to deal with percent moisture by weight ( $M$ ), rather than the concentration of moisture ( $c$ ). Fick's first and second laws are restated as:

$$\phi = \frac{D_z \rho}{100} \frac{\partial M}{\partial z} \quad \frac{\partial M}{\partial t} = D_z \frac{\partial^2 M}{\partial z^2}$$

$\rho$  = density, mass/volume

$M$  = "moisture content"

$$M = \frac{(\text{current weight}) - (\text{dry weight})}{(\text{dry weight})} \times 100\%$$

# Predicting Moisture Diffusion

- Temperature dependency of diffusion coefficient for solids (i.e., ply and core paper) assumed to follow a Arrhenius-type relationship:

$$D = D_o \exp\left(-\frac{E}{T}\right)$$

where:  $D_o$ ,  $E$  = known material constants  
(differ for ply and core  
paper)

$T$  = absolute temperature

# Predicting Moisture Diffusion

- Temperature dependency of diffusion of H<sub>2</sub>O vapor in air assumed to follow a power law of the form\*:

$$D_{air} = 0.03376 \left( \frac{T(^{\circ}R)}{491.67(^{\circ}R)} \right)^{1.81} \frac{in^2}{sec}$$

\* Massman, W.J., *Atmospheric Environment*, Vol 32 (6), pp 1111-1127 (1998).

# Predicting Moisture Diffusion

## *Estimated Core Density and Diffusivity*

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$$\rho_{core} = (V_{air})(\rho_{air}) + (V_{paper})(\rho_{paper})$$

$$D_{core} = (V_{air})(D_{air}) + (V_{paper})(D_{paper})$$

# Predicting Moisture Diffusion

The moisture content ( $M$ ) of any surface layer in contact with air can be related to the relative humidity according to (Springer, 1980):

$$M = M_u \left( \frac{\%RH}{100} \right)^b$$

- constant  $M_u$  = material property
- exponent  $b = 1$  for most materials
- relationship used to define the boundary condition at all ply interfaces



# Predicting Moisture Diffusion

Preceding relations allows forward-difference solution to Fick's equations; summary

- (At all interior ply interfaces) moisture flux leaving ply  $k$  must equal moisture flux entering ply  $k+1$

$$M = M_u \left( \frac{\%RH}{100} \right)$$

- (Boundary conditions):
- (Initial conditions): Initial through-thickness moisture content assumed uniform (assumed = zero in '03)
- Time step increment of 1 minute

# Predicting Moisture Diffusion

## Properties Used in '03

Property	Gr/Ep (typical values)	Type 410, 2-mil Nomex (www.matweb.com)
$D_o$	0.010 $in^2/sec$ <i>(see note)</i>	0.006 $in^2/sec$
$E$	10300 °R	9000 °R
$M_u$	0.02	0.03
Density, $\rho$	0.054 $lbm/in^3$	0.026 $lbm/in^3$

**Note:** Properties reported for Gr/Ep vary widely. For example:  
 $0.005 < D_o < 0.040 \text{ in}^2/sec$

# Predicting Condensation

*Having calculated the moisture content and temperature within core following Step 1, then*

1. Calculate relative humidity within core volume (based on rule of mixtures approximation)

$$\%RH = M_{core} / M_u^{core} = \left( \frac{M_{core}}{V_{air} + M_u^{pap} V_{pap}} \right)$$

# Predicting Condensation (cont'd)

2. Use Clapeyron equation to estimate saturated vapor pressure ( $P_{svp}$ ) at Step 1 core temperatures

$$T_{cor}^{s1} \quad P_{svp} \approx P_{svp}^{ref} \exp \left[ \frac{h_{fg} (T_{cor}^{s1} - T^{ref})}{(RT^{ref})T_{cor}^{s1}} \right]$$

$T^{ref}$  = ref temperature (e.g.,  $T^{ref} = 70^\circ\text{F} = 529.67^\circ\text{R}$ )

$P_{svp}^{ref}$  = saturated vapor pressure at  $T^{ref}$

= 0.3632 psi at  $T^{ref} = 529.67^\circ\text{R}$

$h_{fg}$  = enthalpy of vaporization at  $T^{ref}$

= 1054 BTU/lbm = 820E3 ft - lbf / lbm at  $T^{ref} = 529.67^\circ\text{R}$

$R$  = gas constant for water vapor = 85.76 ft - lbf / lbm - R

# Predicting Condensation (cont'd)

3. Calculate partial pressure of water vapor at Step 1 temperatures:

$$P_{pp} = (\%RH)(P_{svp})$$

# Predicting Condensation (cont'd)

4. Calculate dew point temperature based on reference temperature and partial pressure at step 1 temperatures:

$$T_{dewpt} = \frac{h_{fg} T^{ref}}{h_{fg} - \ln\left(\frac{P_{pp}}{P_{svp}^{ref}}\right) RT^{ref}}$$

# Predicting Condensation (cont'd)

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5. Finally, condensation is predicted if core temperatures during step 2 become lower than calculated dew point temperature

$$T_{cor}^{s2} < T_{dewpt} \Rightarrow \text{Condensation}$$